Thermoforming 2006
16th Annual Thermoforming Conference
September 17th – 20th, 2006
Nashville 2006

“Creativity & Innovation in Thermoforming”

NASHVILLE CONVENTION CENTER
RENAISSANCE HOTEL
NASHVILLE, TENNESSEE

For More Information:
Conference Chairman: Dr. Martin Stephenson, Placon Corporation
608.275.7215  Fax 608.278.4423
mstep@placon.com

Technical Chairman: Mike Lowery, Premier Plastics
414.423.5940  Fax 414.423.5930
mikel@lowerytech.com

Parts Competition Chairman: James Alongi, Maac Machinery
630.665.1700  Fax 630.665.7799
jalongi@maacmachinery.com

Conference Coordinator: Gwen Mathis
706.235.9298  Fax 706.295.4276
gmathis224@aol.com

CHECK OUT OUR WEBSITES AT:
http://www.4spe.org/communities/divisions/d25.php
www.thermoformingdivision.com
I would like to take this opportunity to invite you to the 16th Annual SPE Thermoforming Conference to be held in “Music City” – Nashville, Tennessee. Many of you have requested a Sunday evening start as opposed to the usual Saturday night. In response to this request, the 2006 Conference will kick off on Sunday evening, September 17th and go through Wednesday, September 20th, 2006 with a theme of “Creativity and Innovation in Thermoforming.” This will be our third time in the “Music City” and we are glad to be back in Nashville! The 1998 and 2002 conferences were well attended and highly rated and we know that the 2006 Conference will be no exception!

Planning for the conference has already begun. Mike Lowery (Premier Plastics), Technical Chair for 2006, and I are very excited about the direction of our program. We have already lined up speakers from North America and Europe to conduct both seminars and joint sessions. Many people in our industry are very creative and innovative and we are working to bring them to speak in Nashville. Topics we will cover will be competing in today’s hotly competitive global market, dealing with issues of cost vs. value, and the technical aspects of innovations in the Thermoforming Industry, i.e. material processing, tooling technology, and machinery. This is an excellent forum to launch your new products and conduct business with the leaders of the thermoforming industry.

The convention center in Nashville is a very dynamic location with friendly people to tailor to your needs. We think 2006 will be our largest show ever, so reserve your space now to exhibit. If your company has never sponsored before, we invite you to look at the value one gets by sponsoring. We do have a lottery to draw the sponsors due to the response we get each year. It is a great value! Even if you are not drawn as a sponsor, you will move down to the top of the list to select your exhibit space. Our SPE Thermoforming Board is grateful for the continuous support our sponsors and exhibitors give us each year. We could not do it without you!

Nashville is a very economical venue so that companies can bring CEOs, Sales/Marketing Executives, along with their Engineering and Operations people. This year’s Conference aims to have a particular orientation toward the men and women in the trenches (Engineering and Operations) of the Thermoforming Industry.

It is never too soon to reserve your space for 2006. Gwen Mathis, Conference Coordinator, is happy to help you. Please call her at 706.235.9298, (fax) 706.295.4275 or e-mail: gmathis224@aol.com.

The bands are warming up and awaiting your arrival to the Music City. I am ready and hope to see you in Nashville for a successful Conference in 2006!
The 16th Annual Thermoforming Conference and Exhibition – “Thermoforming 2006: Creativity & Innovation in Thermoforming” – plans are beginning to take shape. This show will be a forum for the newest techniques, latest equipment, materials, auxiliary equipment and current industry news. As an Exhibitor, this event will enable you to showcase your products and services at the only show geared just to THERMOFORMERS! If your company sells to THERMOFORMERS, then this is the place you must be. This industry event is a prime opportunity for you to reach the decision makers in the field and create a brighter future for your business as well.

Full exhibits will be offered. Our machinery section continues to grow each year. If you are not participating in our machinery section, you are encouraged to do so. Each 10’ x 10’ booth is fully piped, draped, carpeted and a sign will be provided. As an extra value, one comp full registration is included with every booth sold. This gives your attendees access to all Technical Sessions, Workshops, Special Events, Plant Tours and all meals. A great bargain at $2,250.00.

Where else can you make personal contact with more than 1,000 individuals who are directly involved with our industry. Your SPONSORSHIP or participation as an EXHIBITOR has demonstrated its potential to help your sales and it is contributing to the strength and success of our industry as a whole.

We urge you to join us at THERMOFORMING 2006 in Nashville! Reserve your space early to avoid disappointment. Booth assignments are made on a first come, first serve basis.

Should you have questions, please call (706) 235-9298, fax (706) 295-4276 or e-mail to gmathis224@aol.com.
EXHIBIT GUIDELINES

EXHIBITOR PACKAGE: $2,250

10' x 10' Booth, Piped, Drape, Sign and Carpet provided. Additional booth spaces: 2nd $2,000, 3 or more $1,750 each.

All Exhibit packages include the cost of (1) Full Conference registration which includes all meals to a company representative. One is given for each booth purchased. All additional attendees must be registered and pay full conference registration to staff your exhibit.

Exhibitors must arrange for any additional services or needs in advance with the designated decorating service. Exhibitor packet will be sent no later than June 1st, 2006.

Parts Competition and Plastics Van to be located in Exhibit area.

Ribbon Cutting Opening Exhibits on Sunday, September 17th, 2006 followed by Welcome Reception on Exhibit floor.

2006 THERMOFORMING CONFERENCE

Creativity & Innovation in Thermoforming

September 17th - 20th, 2006
Nashville, Tennessee

EXHIBITOR REGISTRATION FORM
(Please complete and return with your check today.)

_____ YES, we want to be a 2006 Thermoforming Exhibitor. Enclosed is our check for $2,250. Additional 10’ x 10’ booths as needed will be 2nd $2,000, 3 or more $1,750 each. We will require _______ Booths. We understand that space assignments will be assigned after Sponsors have been selected. Cancellations will be accepted up to June 1st, 2006.

COMPANY NAME: _______________________________________________________________

CONTACT: ________________________________ SIGNATURE: ___________________________

ADDRESS: ______________________________________________________________________

CITY/STATE/ZIP: ________________________________________________________________

PHONE: _______ FAX: _______________________E-MAIL:_____________________________

To properly plan exhibit or badge needs, please list everyone who will be attending. For each exhibit space purchased, a complimentary registration is included ($295 value). All other persons must be registered for the full conference which includes all meals.

Name: ________________________________ Name: _________________________________
Name: ________________________________ Name: _________________________________

MAKE CHECKS PAYABLE TO: 2006 SPE THERMOFORMING CONFERENCE

MAIL TO: GWEN MATHIS, CONFERENCE COORDINATOR
SPE THERMOFORMING DIVISION
P. O. BOX 471, 124 AVENUE D, SE
LINDALE, GEORGIA 30147-0471
FAX (706) 295-4276
### EXHIBITORS
(Signed Up at Press Time)

**“Creativity & Innovation in Thermoforming”**

*DENOTES 2006 SPONSORS*

If your company name is not listed here, please get your form in to reserve your space. Contact Gwen Mathis at 706.235.9298.

**COMPANY**

| * Alcoa Kama Corporation                  |
| * Allen Extruders                          |
| * American Tool & Engineering, Inc.       |
| * Aristech Acrylics LLC                   |
| * Brown Machine LLC                        |
| * Castek Aluminum                          |
| Ensinger/Penn Fibre                        |
| * ExTech Plastics                          |
| * Geiss Thermoforming USA LLC             |
| * Kiefel Technologies, Inc.               |
| Klockner Pentaplast                        |
| * Land Instruments International          |
| * Maac Machinery Company                   |
| * New Hampshire Plastics                   |
| * Onsrud Cutter                            |
| Plastimach Corporation                     |
| * Portage Casting & Mold, Inc.             |
| * Premier Material Concepts                |
| * Primex Plastics Corporation              |
| * PTi (Processing Technologies, Inc.)      |
| Producto Company                           |
| * Raytek Corporation                       |
| * Robotic Production Technology            |
| * Sencorp, Inc.                            |
| * Senoplast USA                            |
| Society of Plastics Engineers             |
| * Spartech Plastics                        |
| Stopol, Inc.                               |
| Thermoformer Parts Suppliers              |
| * Thermwood Corporation                    |
| * Tooling Technology LLC                   |
| * Total Industries International          |
| Zed Industries                             |
2006 THERMOFORMING CONFERENCE
Creativity & Innovation in Thermoforming
Tentative Technical Program Announced
Nashville Convention Center

MONDAY,
SEPTEMBER 18th, 2006

Mini-Seminar in Advanced Topics in Thermoforming - 3 Hours (Limited to 25 attendees) - Dr. James Throne, Sherwood Technologies, Inc.

This 3-hour advanced seminar is designed for the technologist who needs to know how the major engineering aspects such as heat transfer, rheology, interfacial mechanics, and fracture mechanics are applied to thermoforming.

Attendees should consider this as a graduate-level seminar that assumes a thorough undergraduate working knowledge of engineering concepts and mathematics through calculus. If you do not have this background, do not attend.

Please note that attendance is restricted to 25. A waiting list will be available for late registrants.

Not all topics given in the following list will be covered, additional topics may be added, and those that will be covered will be at the discretion of the instructor.

- The Technology of Sheet Heating
  - Understanding the Fundamentals Behind the Energy Dome
  - Radiant Transparency
  - Heating Sagging Sheet

- Mechanics of Sheet Stretching
  - Elastic Modulus and the Forming Window
  - Catenary and Elliptical Catenoid Models for Sag
  - K-BKZ Model – What and Why?
  - Melt Strain Hardening and the Stress Growth Function
  - Finite Element Analysis and Other Methods of Determining Wall Thickness

- Mechanics of Plug Assist
  - Plane Strain vs. Biaxial Strain
  - Plug-Sheet Interfacial Concerns

- Trimming as Fracture Mechanics

- “Development in Infrared Lamp Technology for Thermoforming” - Jerome Martinache, ITM-Application Group Leader, Phillips Special Lighting

- “Match Metal Trim for Thin Gauge” - Bill Hilts, Ontario Die Corporation

- “Technology Does Not Have to be Expensive” - Scott Crandall, Director of Quality & Advanced Technology, McClarin Plastics, Inc.

- “Mold Temperature Control” - TBD

- “Legislative Update” - TBD

- “Business/Casualty Insurance Issues in the Thermoforming Industry” - TBD

- “Product/Company Branding” - TBD

- “Innovation: The Risks and Rewards” - TBD

- “Global View of the Resin Market” - TBD

TUESDAY,
SEPTEMBER 19th, 2006

- “Improving the Thermoformability of Polypropylene by Modification of the Crystal Phase” - Dr. Phil Jacoby, Vice President of Technology, Mayzo Corporation

- “Trends in Thermoform-Tooling in Europe” - Hubert Kittelmann, Marbach

- “Heaters: How, When, Cost” - Frank Wilson, WECO and Ceramicx - Ireland

- “Measuring Plug to Sheet Interactions During the Thermoforming Process” - Noel Tessier, CMT Materials; Tom Gallagher, Sunoco Chemicals

- “Bio-Materials Outlook” - TBD

- “Bringing PHB to the Plastics Industry: A New Family of High Performing Environmentally Friendly Plastics” - Daniel Gilliland, Metabolix
Workshops

2006 Thermoforming Conference
Nashville, Tennessee

** Attendees can only select one of the four workshops being offered. You must register for the conference to attend workshops. **

SUNDAY, SEPTEMBER 17th, 2006

RENAISSANCE HOTEL - MUSIC CITY BALLROOM
8:30 a.m. - 3:00 p.m. – McConnell - Buckel Cut Sheet Workshop

Bill McConnell
Art Buckel

I. INTRODUCTION
• Advantages and Disadvantages of the Thermoforming Process

II. HEATING REQUIREMENTS
A. The Thermoforming Environment
• Plant & Warehouse
• Machine Locations
• Environment Around Machines
B. Types of Heat – Advantages & Disadvantages
• Convection
• Conduction
• Radiation
• How to Obtain Uniform and/or Profiled Sheet Temperature
• “K” Factors and Relative Rates of Heat Transfer
• Regrind & Heat

III. VACUUM & COMPRESSED AIR SYSTEMS
C. Vacuum Requirements
• Why Fast Vacuum Needed
• Vacuum Pressure Measurements
• Surge Tanks
D. Compressed Air Requirements
E. Hydraulic Platens

IV. FORMING TECHNIQUES – BASIC THERMOFORMING METHODS
A. Vacuum Forming
B. Pressure Forming
C. Mechanical Forming
D. Prestretch Forming – For Better Material Distribution
• Vacuum Snapback
• Plug Assist
• Chamber Forming
E. Twin Sheet Forming
F. WRAP UP

Limited to 150 - you must register to attend.

RENAISSANCE HOTEL - FISK ROOM
9:00 a.m. - 4:00 p.m. – Throne Roll Fed Workshop

This basic workshop introduces the various aspects of thin-gauge thermoforming, from materials to machinery, from processing aspects through trimming, to part and old design. A workshop notebook will be provided.

The following will be discussed:
1. General aspects of thin-gauge thermoforming
2. Machine elements
3. Materials
   Polymers
   Additives
4. New materials to be considered
   Biopolymers
   Nanocomposites
5. The importance of sheet extrusion parameters
6. Heating the sheet
7. Forming the sheet
8. Trimming
9. Molds and mold design
   Mold materials
   Plug materials
10. Part design concepts
    Wall thickness determination
    Corners
    Coining
    Plug design
**Workshops**

2006 Thermoforming Conference
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11. Regrind considerations
12. Foam forming
13. Production monitoring and control
   Temperance
   Birefringence
14. Lingering concerns

**James L. Throne:** Jim Throne is President, Sherwood Technologies, Inc., Dunedin, FL., a consultancy focusing on advanced plastics processing technologies, including thermoforming, foam processing and rotational molding. He is Fellow of the SPE and Fellow of IoM® (England). He was SPE Thermoformer of the Year 2000. He was honored by the SPE European Thermoforming Division 2004 for his technical contributions to the worldwide thermoforming industry. He has published 10 books in polymer processing, including four in thermoforming. He holds nine U.S. patents, including a fundamental one in thermoforming CPET. He has written more than a dozen technical book chapters and has published and presented nearly 200 technical papers. He is current Technical Editor of SPE Thermoforming Quarterly. He is Fellow of the Society of Plastics Engineers and Fellow of Institute of Materials, Mining and Manufacturing (IoM®).

Limited to 150 - you must register to attend.

**Michelle Curenton:** Michelle currently serves as a Sales/Product Engineer with FACTS, Inc., a supplier of closed-loop controls systems for extruders, mixers, calenders and thermoformers. She has spent ten years with the company, which exclusively serves the plastics and rubber industries. During this time she has worked as a project and process engineer, managed many start-up projects and custom installations, and routinely helps clients with trouble-shooting or diagnostic issues. She is often called upon to support the company with technical presentations and has presented several papers at industry conferences and SPE meetings. Michelle holds an electrical engineering degree from The University of Akron. Prior to joining FACTS, she worked for a leading company in the steel industry in several engineering roles. In addition to electrical/project engineering skills, she has a strong IT background and combines process data with a clear understanding of software/hardware capabilities, including ERP and SPC applications. She specializes in identifying clients’ processing issues and providing realistic solutions for improved technology and manufacturing practices. Michelle is married and the mother of a son. She resides in NE Ohio and routinely travels the country to work with clients on a variety of integrated line-control projects for plastics or rubber manufacturing.

Limited to 50 - you must register to attend.

**Renaissance Hotel - Belmont One Room**

**9:00 a.m. - 12:00 p.m. – Process Controls Workshop - “Improve Production Capacity of Your Equipment: Use Updated Controls”**

Thermoformer life can be extended and better-quality product can be produced with updated control systems. Learn how temperature, gauge, speed, pressure and downstream equipment can all run based on a product code, with adjustments made automatically based on set points and closed-loop control algorithms (including shot cycle, platen movement, gauge/profile and temperatures). Your firm can reduce scrap, boost throughput, improve quality and consistency with improved controls and by identifying changes with trend charts/graphs and alarming. Data collection is also useful for on-line troubleshooting/diagnostics. This seminar will show you how.

Limited to 50 - you must register to attend.
RENAISSANCE HOTEL - BELMONT ONE ROOM
1:00 p.m. - 4:00 p.m. – How to Do Business in India Workshop

The global economy has mandated international partnerships, India and China emerging as two strong partners. It is in the best interest of our manufacturing industry to at least be aware of what is happening in India and to understand several ways in which we can do business together. The seminar will cover issues related to doing business with/in India including but not limited to Reasons for Exploring Business Opportunities in India, Market Opportunities for U.S. Firms in India, State of Indian Manufacturing, State of Indian Services Sector, Business Destination - Economic and Political, India’s Socio-Cultural Heritage, Challenges to Doing Business in India, U.S. Perception of India’s Future, Future Directions and India’s Economic Policies, Etc. A few case studies will be discussed to learn from experiences.

Dr. Promod Vohra: Dr. Vohra is the dean of the College of Engineering and Engineering Technology (CEET). Dr. Vohra is a graduate faculty and a full professor in the Department of Technology. Prior to becoming the dean he was the associate dean for six years where he boosted enrollment in the college by 45 percent over the last seven years. Before that he was the electrical engineering technology (EET) coordinator in the Department of Technology. Dr. Vohra, in addition to having a doctorate in Instructional Technology (with cognate in Industrial Engineering), has a Masters as well as a Bachelors degree in Electrical Engineering. The BS degree was earned from Delhi College of Engineering, India and the latter two degrees were earned at NIU in 1988 and 1993, respectively. Prior to coming to the field of academia, he worked in industry (Philips) for five years as a technical support engineer. He joined NIU in 1988 as a lecturer, became an assistant professor in 1993, an associate professor in 1995 and the associate dean in 1997.

His interest areas are digital systems, instruction design, industrial training, new technologies and applications of technologies. As the coordinator of the Electrical Engineering Technology (EET) program (1988-1995), he increased the program enrollment more than 800 percent, published several refereed articles and brought in about a million dollars worth of equipment grants to develop and expand EET laboratories. He recently brought in software and other grants worth approximately 22 million dollars. Dr. Vohra has been very active in university service and in regional and national professional committees/organizations. He was the recipient of the 1988 Outstanding Young Alumnus Award in 1995, he was given the Excellence in Undergraduate Teaching Award by Northern Illinois University and in 1996 he received the Outstanding Professor Award in the region (seven professional registrations such as a professional engineering (PE) and a senior certified industrial technologist (CSIT).

Limited to 35 - you must register to attend.
Workshops

2006 Thermoforming Conference
Nashville, Tennessee

**Attendees can choose one only.**

**WEDNESDAY, SEPTEMBER 20TH, 2006**

**Renaissance Hotel - Ryman Room**
8:30 a.m. - 3:00 p.m. – Extrusion Workshop
Presented by the SPE Extrusion Division
Limited to 100 - you must register to attend.

☞ Extrusion Basics - Tim Womer, Xaloy
☞ Co-Extrusion - Gary Oliver, Cloeren
☞ Compounding Extrusion - Paul Anderson, Coperion; Charlie Martin, Leistritz
☞ Reactive Extrusion - Paul Anderson, Coperion; Charlie Martin, Leistritz
☞ Extrusion Troubleshooting - Mark Spalding, Dow Chemical

**Renaissance Hotel - Music City Ballroom**
9:00 a.m. - 12:00 p.m. – Geiss Workshop
Limited to 100 - you must register to attend.

☞ “The Future of the Thermoforming Industry” - Manfred Geiss & Albert Woltron, Geiss USA
SPE THERMOFORMING 2006
NASHVILLE CONVENTION CENTER
2006
REVISED 1-15-06
REV 12
BOoths ARE 10' x 10' UNLESS NOTED
AISLES ARE 10'
We invite you to participate in this year’s Thermoforming Parts Competition and Showcase. This important event is a part of our 2006 SPE Thermoforming Conference in Nashville, Tennessee, September 17th - 20th, 2006. In order to make this year’s Parts Competition and Showcase the best ever, we need your support. Take advantage of this unique opportunity to support your industry, get in front of editors from major publications, and show off your thermoforming skills.

SHOWCASE OF PARTS

The Showcase of Parts was developed as a non-competitive forum to display products from our industry. This year’s showcase will feature past award winning parts, as well as parts not involved in the competition. We also encourage any thermoformer, machinery manufacturer, material supplier, and attendee to share parts with us. This will be a show and tell area for all to promote their parts. Items of interest in the industry like thermoforming versus other processes, new materials, or environmental issues are encouraged. Do you have a success story to share with us?

Cut Sheet Parts Competition

The following Categories will be Judged:
Automotive
Consumer Products
Twin Sheet Product
Multi-Part Assembly
Electronic Products
Industrial Application
Point of Purchase

Roll-Fed Parts Competition

The following Categories will be Judged:
Consumer Packaging
Consumer Housewares
Critical Barrier
Consumer Electronics
Food Container
Industrial Packaging

Best International Part
PEOPLE’S CHOICE AWARD
This award is voted on by the attendees and exhibitors of the SPE Thermoforming Conference. Ballots are provided at the Conference registration and the ballot box is located in the Parts Competition Pavilion. One entry per person. The award is presented at the Parts Competition Awards Dinner on Tuesday, September 19th, 2006.

JUDGING
The judging will be conducted by a panel of six industry professionals, from both the cut sheet and roll fed industries. The judges will have extensive knowledge of all aspects of the thermoforming process. A minimum of 3 entries per category is required for an award to be presented.

JUDGING CRITERIA
The judging criteria will include technical mastery, surface finish, distinct quality, market viability (compared to other processes), originality, material difficulty, mold complexity, and secondary operations. All entries will remain anonymous until the judging is completed. A part and process write up will be allowed for the judging if it does not include the name of the thermoformer. The parts will be judged based on the process and not the end use of the products.

AWARDS
All participants and award winners will be recognized on Tuesday, September 19th, 2006 at the Parts Competition Awards Dinner at the Renaissance Hotel.

For more information, contact: James Alongi
(630) 665-1700  Fax (630) 665-7999
OFFICIAL ENTRY FORM

16th Annual
Parts Competition and Showcase

☐ Parts Competition  ☐ Showcase Entry

Company: _____________________________________________________________________________________

Address: _______________________________________________________________________________________

City: _______________________________ State: _________________ Zip: ____________ Country:_____________

Company Contact: ______________________________________________________________________________

Telephone: ___________________________________________ Fax: ______________________________________

E-mail: ________________________________________________________________________________________

Entry Specifications:

Category:  ☐ Cut Sheet  ☐ Roll Fed

Parts Description: _______________________________________________________________________________

Material Type: _________________________________ Gauge: __________________ Supplier: _______________

Mold Construction: _______________________________________  Mold Builder: _________________________

Part Description and Unique Challenges for Consideration: __________________________________________

_______________________________________________________________________________________________

_______________________________________________________________________________________________

FOR SHIPMENT UP TO 30 DAYS IN ADVANCE OF SHOW:

Please ship to: Roadway Express
c/o RPM / Complete Expo Parts Competition
3240 Franklin-Limestone Road
Antioch, Tennessee 37013

• Please supply this form with a company labeled photo with each part entry.

• A supplemental sheet can be provided to expand the part description/unique challenges section. Please refrain from mentioning the company name in this section.

• A faxed copy of your entry is required by August 21st, 2006 to Fax: (630) 665-7799.

• CLEARLY LABEL EACH CARTON: SPE PARTS COMPETITION – DO NOT OPEN!

• Parts will be accepted from August 21st to September 11th, 2006.

• Judging will be done prior to opening of show – entries must be received prior to September 11th, 2006.

IF YOU DESIRE TO HAVE YOUR PARTS RETURNED, YOU MUST PROVIDE PACKAGING AND ENCLOSE A PRE-ADDRESSED RETURN LABEL AND PREPAID SHIPPING INSTRUCTIONS.

Signature: ______________________________________________________________  Date: _________________

For more information, please contact James Alongi, Maac Machinery, (630) 665-1700, Fax (630) 665-7799, or email: jalongi@maacmachinery.com.
16th Annual Thermoforming Conference

Nashville 2006

“Creativity & Innovation in Thermoforming”

September 17th – 20th, 2006
Nashville Convention Center
Renaissance Nashville Hotel
Nashville, Tennessee

For Reservations: Call 615.255.8400
Request: SPE Thermoforming Rate of $143.00

**Please note! The hotel will require a deposit of one night’s room and tax at the time the reservation is made. Cancellations made after August 13, 2006 will result in the forfeiture of one night’s deposit. Any reservation made after August 13, 2006 will require a non-refundable one night’s deposit at the time the reservation is made.

Check out our websites at:
http://www.4spe.org/communities/divisions/d25.php
www.thermoformingdivision.com

For Information Contact:

CONFERENCE COORDINATOR:
GWEN MATHIS
706.235.9298 • Fax 706.295.4276
E-mail: gmathis224@aol.com
A NOTE TO PROSPECTIVE AUTHORS

TFQ is an “equal opportunity” publisher! You will note that we have several categories of technical articles, ranging from the super-high tech (sometimes with equations!), to industry practice articles, to book reviews, how to articles, tutorial articles, and so on. Got an article that doesn’t seem to fit in these categories? Send it to Jim Throne, Technical Editor, anyway. He’ll fit it in! He promises. [By the way, if you are submitting an article, Jim would appreciate it on CD-ROM in DOC format. All graphs and photos should be black and white and of sufficient size and contrast to be scannable. Thanks.]
I cannot believe that I have been a member of the SPE Thermoforming Division for 10 years and your Membership Chairman for 8 years. We have been through quite a bit in those years. We have had some amazing highs – Chicago in 1999 – and some unfortunate lows – Milwaukee in 2001. We have had some outstanding growth in both our Conference attendance and in the quality of our Quarterly. We are offering more scholarship and committing to more good deeds. Our industry seems to be really taking off with advancements in automotive, medical packaging and consumer goods. The future of the Thermoforming Industry continues to look bright. The only way to keep up with this fast-moving industry is to continue to support this Division.

The New Year will bring some interesting challenges for all of us. Our Conference will be held September 17th - 20th in Nashville, Tennessee. I think Nashville is my favorite location for our Conference. It has everything you need, good food, great music and plenty to see, right within walking distance. Martin Stephenson is working long hours to bring us a great Conference this year. The technical program is in the capable hands of Mike Lowery. I urge all of you to do anything you can to support this Conference.

If you have any suggestions on how to improve, grow or challenge this Conference, please feel free to contact one of us on the Board. The amount of “good works” we are able to accomplish due to a successful Conference is hard to believe. Please continue to support us, so that we may continue to support and grow our industry.

As always, I ask each and every one of you to continue to support membership. If you know of anyone who may benefit from this Quarterly or from any of the other advantages that membership offers, please let us know. Have a great year and I hope to see you in Nashville.

God bless America!!

MEMBERSHIP REPORT

as of 1/4/06

Primary Paid ....................... 1,144
Secondary Paid ....................... 496
Total Membership .............. 1,640
Goal as of 6/30/2007 ........... 2,000
To Our New Members

Roger E. Blanton
Springfield, Missouri

Thomas E. Brown
Allen Extruders, Inc.

Ron Connell
Alcoa Reynolds Food Packaging

Phillip Crosbie
Marplex
Victoria, Australia

Matthias H. Erhardt
Siemens Energy & Automation
Norcross, Georgia

Brian K. Evenson
Plastica Plus, Inc.
Brainard, Minnesota

Eric Faucher
Marquexz
Montreal, QC - Canada

Ke Feng
GE Plastics
Washington, West Virginia

Joe Green
ManPlas, Ltd.
Stockport, United Kingdom

Jeff Griffin
Eviro Systems, Inc.
Seminole, Oklahoma

Seref Halulu
Saykap As Ikltell, Turkey

Howard J. Kenney
Spartech Plastics
Clayton, Missouri

Youngseok Seiok Kim
Mississauga, Ontario - Canada

Edward Kus
Intermatic, Inc.
Spring Grove, Illinois

Niall Marshall
Kampion Gate
South Africa

Steven L. Masia
SAPPI Fine Paper
Westbrook, Maine

Jason N. Mattia
Alcoa Kama
Hazleton, Pennsylvania

Atul Mehta
New Berlin, Wisconsin

Stephanie Morgan Fisher Stanelco, Inc.
Orlando, Florida

Richard Motill
Proex, Inc.
Batavia, Illinois

Paul J. Nicholson
Signum NZ Ltd.
Greenmount, New Zealand

Thomas S. Pedersen
Rexam Plastics
Containers
Skanderborg, Denmark

Mark Rath
Reynolds Food Packaging
Grove City, Pennsylvania

Doug Shelton
McConkay Company
Summer, Washington

Benjamin W. Smith
Devon, Pennsylvania

Paul W. Tomich
First Choice Packaging
Fremont, Ohio

Bill Trometer
Asheville Thermoform Plastics
Fletcher, North Carolina

Frank Tucker
Als Garden Art Pty Ltd.
Gold Coast, Australia

David Vadney
Pactiv
Canandaigua, New York

WHY JOIN?

It has never been more important to be a member of your professional society than now, in the current climate of change and volatility in the plastics industry. Now, more than ever, the information you access and the personal networks you create can and will directly impact your future and your career.

Active membership in SPE:
• keeps you current
• keeps you informed
• keeps you connected

The question really isn’t “why join?” but …

WHY NOT?
2005 THERMOFORMING PARTS COMPETITION WINNERS

RETraction

We sincerely apologize to Perfecseal, Prent Corporation and Profile Plastics for errors in the Parts Competition Section that were published in the 4th Quarter Thermoforming Quarterly. We regret our mistakes and wish to issue the correct information. ~ Editor

Critical Barrier Package Award

The redesign of packaging for two medical devices, a sling system and a subfascial hammock, was initiated in order to reduce the size of the packaging and to make it possible to denest the trays without the occurrence of tissue interleafing. By rearranging the orientation of the devices, Perfecseal was able to achieve tray-volume reductions of 68% for the sling system and 54% for the subfascial hammock. Additionally, by using C0025 Internal Denest PETG supplied by Pacur, Inc., Perfecseal was able to eliminate the problem of tissue interleafing without requiring a revalidation of the seal parameters, which would have been necessary if a silicone-coated material had been chosen instead.

Perfecseal (A. Demis Co.); 920.303.7129
www.perfecseal.com

Consumer Electronics Award

The packaging for Western Digital’s Portable USB Drive is a unique set of four thermoforms, each with a specific role to play in creating the package. Two static dissipative inner thermoforms snap together to secure the hard drive inside trays that are sealed together using radio frequency (RF). The inner parts are made from 0.020-inch clear Pentastat ASKPET 56 supplied by Klockner Pentaplast of America, Inc., and the trays are made from 0.030-inch clear GAG supplied by Thai Kodama Co. Ltd. ASKPET 56 offers ESD protection for the actual product, and the use of GAG provides the ability to RF seal. This 100% recyclable plastic design meets product-protection requirements while providing product visibility, ESD protection, and shelf appeal. The packages, which afford both front and back views of the product, require less shipping space because they interlock when every other one is rotated 180° in the shipping carton.

Prent Corporation; 608.754.0276; www.prent.com

Roll Fed Competition

Most Unique Package Award

The DePuy Orthopaedics Tempfix External Fixation System package consists of five individual thermoformed parts. Each of three modular inner trays carries one of four different fixation devices, along with the tools for their application. One universal cover snap-fits onto each of the modular inner trays, while one universal outer tray holds and protects any of the inner/cover combinations. Each product tray with cover is loaded into the sealable outer tray for sterilization. The cover provides an area for a graphic feature. All inner trays and cover are formed from .040 Blue Tint PETG. The outer tray is formed from .045 Blue Tint PETG Goex Corp. supplies the materials.

Prent Corp., 608.754.0276; www.prent.com

Multipart Award

The panoramic analog dental X-ray enclosure required a total of nine parts (12 parts for the digital model), all of which were pressure formed into machined aluminum water-cooled, textured molds. The texturing of molds allows for a consistent part finish for all parts and eliminates evidence of sink marks, knit lines, and gate marks that are typically associated with injection molding. Clean part-to-part fit is accomplished with undercuts in the molds, which are pneumatically articulated with solenoids tied into the digital programming logic of the forming machines. Because of the elliptical contours of the enclosure’s design, the undercuts are broken into multiple sections for each side of the parts. Tight process control of molded-in color and texture for consistent part-to-part appearance was required. The material used was 0.187 to 0.375 gauge Kydex T, supplied by Kleerdex Co.

Profile Plastics; 847.604.5100; www.thermoform.com
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Every year The SPE Thermoforming Division selects an individual who has made a outstanding contribution to our industry and awards them the Thermoformer of the Year award.

The award in the past has gone to industry pioneers like Bo Stratton and Sam Shapiro, who were among the first to found thermoforming companies and develop our industry. We have included machine designers and builders Gaylord Brown and Robert Butzko and toolmaker John Greip, individuals who helped develop the equipment and mold ideas we all use today. We have also honored engineers like Lew Blanchard and Stephen Sweig, who developed and patented new methods of thermoforming. Additionally, we have featured educators like Bill McConnell, Jim Throne and Herman R. Osmers, who have both spread the word and were key figures in founding the Thermoforming Division.

We’re looking for more individuals like these and we’re turning to the Thermoforming community to find them. Requirements would include several of the following:

- Founder or Owner of a Thermoforming Company
- Patents Developed
- Is currently active in or recently retired from the Thermoforming Industry
- Is a Processor – or capable of processing
- Someone who developed new markets for or started a new trend or style of Thermoforming
- Significant contributions to the work of the Thermoforming Division Board of Directors
- Has made a significant educational contribution to the Thermoforming Industry.

If you would like to bring someone who meets some or all of these requirements to the attention of the Thermoforming Division, please fill out a nomination form and a one-to two-page biography and forward it to:

Thermoforming Division Awards Committee
% Productive Plastics, Inc.
Hal Gilham
103 West Park Drive
Mt. Laurel, NJ 08045
Tel: 856-778-4300
Fax: 856-234-3310
Email: halg@productiveplastics.com

You can also find the form and see all the past winners at www.thermoformingdivision.com in the Thermoformer of the Year section.

You can submit nominations and bios at any time but please keep in mind our deadline for submissions is no later than December 1st of each year, so nominations received after that time will go forward to the next year.

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Presented at the September 2007 Thermoforming Conference in Cincinnati, Ohio

The Awards Committee is now accepting nominations for the 2007 THERMOFORMER OF THE YEAR. Please help us by identifying worthy candidates. This prestigious honor will be awarded to a member of our industry that has made a significant contribution to the Thermoforming Industry in a Technical, Educational, or Management aspect of Thermoforming. Nominees will be evaluated and voted on by the Thermoforming Board of Directors at the Winter 2007 meeting. The deadline for submitting nominations is December 1st, 2006. Please complete the form below and include all biographical information.

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• Publications and patents (please attach list).
• Evaluation of the effect of this individual’s achievement on technology and progress of the plastics industry. (To support nomination, attach substantial documentation of these achievements.)
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Please submit all nominations to: Hal Gilham, Productive Plastics, 103 West Park Drive Mt. Laurel, New Jersey 08045
Placon Corporation, now in its 40th year, was the dream and is still the passion of entrepreneur and engineer Tom Mohs.

Headquartered in Madison, Wisconsin, Placon is a global thermoformer, supplying customers on four continents with well-designed, quality manufactured thermoforms. Placon services its global customers from three facilities – Madison, WI; Loves Park, IL; and Suzhou, China.

Company revenues exceeded $85 million in 2005 through the efforts of nearly 350 team members.

Tom Mohs, who today is the corporation’s Chairman, is one of the industry’s original entrepreneurs. Tom’s keen interest in plastics and plastics processing were evident early on in his life when he led an effort as a student at the UW-Madison’s College of Engineering, to convince the Dean to support a plastics processing course in its curriculum and he succeeded.

After graduation, Tom went to work in product development with the Plax Corporation in Connecticut. There, he applied his plastics processing knowledge and design skills to creating new products, particularly thermoformed plastic products. Tom was one of the original developers of the thermoformed high impact polystyrene dairy container and lid.

Always having had an interest in starting his own enterprise, Tom decided after four years to return to his hometown and start a custom thermoforming business. He had a lot of ideas for new thermoformed products and focused on designing them to efficiently serve their functions. He brought revolutionary ideas to product and tooling design, thermoformer design and processing. He took on the tougher design applications and put forth the effort needed to further the capabilities of the industry.

Today, the company’s tagline “Better Design. Better Packaging.” ensures the original intent of its founder.

Placon remains privately held by Tom and his family, and stays true to its founder’s solid Midwestern values. Tom’s greatest desire is that Placon team members can feel proud to work at Placon and, as a result of being part of the organization, can achieve their own personal development and success.

Placon today is a thriving corporation listed in the top 20 in the industry and is driving toward its goal to become a Top 10 North American Thermoformer by 2010. In achieving this goal, the company believes it will position itself to be able to remain privately-held and continue to determine its own destiny through the next generation.

Placon’s primary markets are in food, retail and medical packaging. The company continues to invest in the industry’s latest technologies in equipment and operating systems, so that it is capable of continuing to offer its customers what they need to succeed and lead in their markets.

Placon will continue to expand geographically to support its customers’ regional needs. Placon opened its first operation in China in December of 2004 to service its retail customer base who, to remain globally competitive, had to move their manufacturing operations to Asia. Outside of Madison and Loves Park, Placon expects to continue its geographic expansion in North America in the upcoming years before 2010.
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Wednesday, May 3rd, 2006
Executive Committee Arrive
Technical Chairs Arrive

Thursday, May 4th, 2006
7:30 am – 8:00 am – Breakfast
8:00 am – 10:00 am – Technical Chairs Meet with Executive Committee
10:00 am – 5:00 p.m. – Executive Committee Meeting
11:00 am – Noon – James Alongi, Finance Committee Meet with Executive Committee

Friday, May 5th, 2006
9:00 am – 11:00 am – Materials Committee - Promenade 1
9:00 am – 11:00 am – Machinery Committee - Promenade 8
9:00 am – 11:00 am – Processing Committee - Captain’s Galley A
12:00 pm – 1:00 pm – Lunch - Captain’s Galley B
1:00 pm – 5:00 pm – All Other Committees - Captain’s Galley B
6:00 pm – Board Dinner Off Site - TBD

Saturday, May 6th, 2006
7:30 am – 8:30 am – Breakfast – Promenade 8
8:30 am – Noon – Board of Directors Meeting - Promenade 6-7
Golf to be arranged by Joe Peters

Sunday, May 7th, 2006
Depart
Abstract

The demand for large parts with thick walls, constructed of multiple polymer layers, along with the desire for quick turn-around time, lower tooling cost, and low-pressure processing is making thermoforming very attractive v. injection molding. Despite the long history, thermoforming is still very much an art rather than a science. There are very few reliable tests available to processes and researchers for analyzing and quantifying thermoformability. This paper presents a comparison between current methods and a novel test apparatus that closely simulates the thermoforming process under controllable conditions while collecting quantitative information, which can be used to assess, compare, optimize, or predict thermoformability of given plastic materials.

Introduction

Thermoforming is a widely used process to produce deep arts of various wall thickness and surface textures. Production is very cost-effective with respect to tooling and machine costs and modern machines can achieve high output rates. In principle, thermoforming is a simple process of stretching heating plastic sheet over or into a mold cavity. Theoretically, the ability of a plastic material to be shaped by thermoforming depends on the rate of change of strength or modulus with the change in strain rate and temperature (1). In reality, the process is a complex interplay between polymer molecular weight (MW), molecular weight distribution (MWD), crystallinity, density, thermal conductivity, and temperature-dependent melt viscosity and melt elasticity. Another variable, which may influence thermoformability, is the processing history of the extruded sheet stock. The larger the part and the thicker the wall become, the more complex is the effect of these factors during and after the forming process. Significant hands-on experience is required to make new polymeric materials work.

Unlike other processes, thermoforming requires flat sheet, not pellets, as feedstock. So any material intended for thermoforming must be first converted into sheet. Depending on the process of making sheet, process conditions, process rates, amount of regrind, and storage conditions, the feedstock may vary in its thermal stress distribution, within and between lots. This can create a real blind spot, which converters overcome by on-line adjustment of the thermoforming process parameters. The situation can be even more complex if the extruded sheet consists of more than one plastic, with dissimilar natures, or with one side of the sheet grained or textured. For most other processes, judicious use of the simple melt flow rate test can help processors solve many of the processing and quality related issues.

This is not the case with thermoforming. Actual determination of thermoformability through field trials can be very expensive. What test will one use to make sure whether or not a new material will thermoform satisfactorily? How does one learn about lot-to-lot or within-lot variations? How does one accommodate known variations? There is no easy-to-use, repeatable, yet comprehensive test to rescue converters, especially when a new material or supplier is involved.

Several tests (2) are available, some of which are very crude, qualitative, easy to understand but not...
repeatable. Others are highly analytical, expensive and difficult to comprehend. The following is a review of some of these tests.

**Sag test** (3). Sag is the temperature-dependent measure of tensile strength and sheet geometry. This is the most commonly used test, which simulates hot creep under no external load. A flat sheet is clamped in a frame and heated to a forming temperature inside a forced air oven or by radiant heaters. The time required for the heated sheet to sag to a fixed distance is reported as sag resistance. This test is a useful first step but the results depend on how the sample is clamped (circular window v. rectangular window, cantilever v. all sides clamped), sheet weight, method of heating, surface area, and sheet thickness. It is often not repeatable and does not provide any clue about melt elasticity, i.e., how the heated sheet will react to external stresses in, say, plug-assisted forming. The plastic may have a very high sag resistance but may have no ability to form at all.

**Hot tensile/creep test** (4). As the polymer temperature increases, its strength and modulus decrease and elongation increases. Thermoforming occurs in the rubbery plateau, at temperatures above the glass transition temperature, Tg. The broader the rubbery plateau and the higher the polymer modulus at the forming temperature, the better the thermoformability. In this test, a specimen is die-cut from the extruded sheet. It is heated to the desired temperature in a forced air environmental chamber and is stretched at constant speed. The tensile modulus or strength is plotted against strain. Even though quantitative in nature, hot tensile tests are difficult to carry out with any degree of reliability. At elevated temperatures, stretching is not confined to the neck-down portion, and grip-slip or grip-extrusion is common. Slow heating rates may induce annealing.

Hot creep tests are more sensitive than hot tensile tests to changes in polymer character. Further, heat is conducted to the load cell, affecting the accuracy.

Neither test truly replicates biaxial stretching under rapid speed (>20 mm/sec), and heat transfer between the mold and the heated plastic sheet that is so common even in the simplest thermoforming process is not present in either test.

**Dynamic rheological tests.** Dynamic mechanical testing is used to determine the storage or elastic modulus (G') and the loss or viscous modulus (G'') as functions of temperature or strain rate. This test requires less material than those given above, can be done rapidly, and the results are highly repeatable. The data provide indirect information about MD and MWD, as well as direct information of the complex modulus as a function of temperature (5). Higher zero shear viscosity, broader MWD, and higher modulus at the forming temperature are considered to be favorable attributes of a polymer. However, the test equipment is expensive and requires a trained person to run the test and interpret the data. Most importantly, it does not reflect the variables in the thermoforming process.

The thermoforming process can be simulated through the stress relaxation experiment (6). In this test, stress is applied to the plastic and the decay in stress relaxation is measured. Stress relaxation time is reported to increase linearly with sag resistance (5). However, at elevated temperatures at high-applied stress levels, the creep rates are very high, making interpretation of the creep data difficult. In addition, the stress relaxation constant varies with the test parameters selected.

**Melt tension test.** In this test, the plastic is melted, extruded into a fiber, and the fiber is stretched at constant velocity. One device that performs this test is the Rheotan attached to a capillary rheometer. The test is repeated at various velocities. The force and velocity at which the fiber breaks are reported as melt strength and draw velocity. Even though this test is useful, it is not very representative of the thermoforming process. First, the process is done above the melt temperature of the polymer, while most thermoforming is done in the rubbery region of the polymer. Thus, all information relating to sheet extrusion parameters are lost during the melting step. Fiber is one-dimensional while thin sheet is two-dimensional and thick sheet is three-dimensional. The draw strength and velocity can vary with the way in which the fiber is cooled. Further, some plastics tend to strengthen by stretching in one dimension. This is a simple test and results are easy to interpret, but the data do not correlate well with the forming process variables.

(continued on next page)
Numerical methods\(^{(7)}\). There are computational tools which numerically simulate thermoforming and predict response to input variables. However, these methods, like most numerical simulation methods, are based on simplified assumptions, and require values of many polymer characteristics, many of which are not readily available or are expensive to obtain. The free surface flow involved and the complexity of modeling melt elasticity make these models less reliable.

In absence of any real, easy-to-use and easy-to-interpret test method, one must resort to actual thermoforming. This may require a large amount of plastic sheet, time, and money. Results of one trial may not always be applicable to actual production. Therefore, we propose a method that overcomes many of these obstacles.

Proposed Equipment

As shown in Figure 1, the proposed automated equipment is a miniature version of actual thermoforming machine and incorporates all essential unit steps—heating, forming, and cooling. It uses 4-inch x 4-inch square sample of desired thickness, preferably die-cut from extruded feedstock, but it can also be injection or compression molded. Most quality control labs have 8-inch x 8-inch heated compression presses and injection molding machines. The sample is clamped between two insulated plates, and the tray is manually placed on the loading rail.

A software input menu includes the selection of the forming method, forming temperature, heating rate, heat soak time, ram speed, cooling time, maximum force, and the maximum draw depth. Once activated, the sample tray moves to the heating station where two infrared or ceramic heaters heat the sample from above and below. Both heaters can be programmed independently and can be positioned at desired distances from the sample surfaces. A non-contact, laser-guided infrared temperature probe continuously measures the surface temperature.

When the sheet reaches the preset surface temperature, or the preset temperature and heat soak time, the tray moves to the forming station in less than a second. A plunger, equipped with a male plug descends into the sheet at a preprogrammed speed. The force required to deform the heated sheet is continuously measured by a load cell mounted on the top of the plug. The computer interface captures the force data and plots it as a function of either the distance from the surface or time.

As soon as either the preset force is reached or the sheet is deformed to a preprogrammed distance, a fan is activated to cool the sample for a preprogrammed time. At the end of the cooling time, the plunger retracts and the tray carrying the cold, formed part is returned to the loading station. The part is then manually removed from the tray, inspected for wall thinning, tearing, blisters, burn marks, loss of grain or texture, loss of gloss, fading, and so on. Thickness is manually measured and the thickness distribution recorded.

The equipment and software allow selection of pressure forming, vacuum forming, or vacuum-assisted pressure forming.

The force data can either be used as is or with suitable software, can be converted into a predictive model.

The equipment overcomes several problems of earlier methods:

- It uses a small amount of sample, either from existing feedstock or made using available quality control equipment.
- It heats material rapidly but under controllable conditions. This allows mimicking actual thermoforming conditions. Further, the top and bottom of the sheet can be heated to different temperatures either by adjusting the distance.
of the heaters to the sheet or by adjusting the heating rates. This is helpful when coextruded sheets are used.

- The force is measured using an accurate load cell while the sample is losing heat, as is typical of the actual thermoforming process.
- The ability to change forming speed can be useful in studying the effect of increased line speed.
- The unit allows changes in plug geometry and type of plug material, simulating the effect of plug materials.
- Once the part is formed, it is cooled under controlled conditions to determine the effect of cooling on shrinkage, warpage, grain distortion, gloss variation, and so on. These observations cannot be made in any of the aforementioned methods.
- The equipment is as easy to use as the melt flow indexer and it provides quantitative data under controlled conditions, which can be repeated.

**Test Results**

Extruded sheets of nylon, HDPE, ABS, PP, PC, PVC, PMMA, POM, HIPS, PETG, filled TPO, and HMS-TPO were obtained from suppliers. Samples were cut from various feedstocks and thermoformed using a 100 mm long, 50 mm diameter, 30-degree truncated cone plug under various plug speeds and sheet temperatures.

Figure 2 shows the relationship between the forming force and depth of draw at 150°C for several polymers. The required force increases with increase in melt strength. Polymers with true strain hardening show an increase in the force required with increasing draw depth, as seen for POM in Figure 3. For crystalline polymers, an increase in force at the deepest draws is due to the cooling of the sheet as it contacts the cold plug. The sag distance can be estimated from the depth of penetration of the plug before the transducer measures a non-zero force.

Figure 4 shows the effect of sheet temperature on the force required to form various polymers to a draw depth of 100 mm at 20 mm/second using the truncated cone plug. As seen for most
amorphous materials such as ABS, HIPS, PMMA, PVC and PETG, the force decreases nearly linearly with sheet temperature. For crystalline polymers, the force does not decrease linearly. For HDPE and PP, a step change in the force occurs around the polymer melt temperature. For nylon and PC, the force actually increases around their melt temperatures.²

Figures 5a and 5b show the effect of temperature on the forming characteristics of talc-filled TPO and HMS-TPO. The TPOs have similar tensile strengths and moduli at room temperature. HMS-TPO does not show a loss in melt strength while the filled TPO does. Figure 5c shows the effect of test speed on the forming characteristics of these two polyolefins. At high speeds, the filled TPO shows substantial loss in melt strength whereas the HMS-TPO shows very little change in the same temperature range. The increase in stress at greater deformation indicates a strain-hardening effect.

Figure 6 shows the tensile strength v. temperature for these two TPOs, measured at a 50-mm/min crosshead speed. The HMS-TPO has a much higher tensile strength than that for the filled TPO.

Conclusions

The current test methods reviewed above do not encompass the wide range of variables found in even the simplest of thermoforming processes. The proposed novel device has demonstrated its use in determining the thermoformability of many polymer materials. Quality control, process engineering, raw material suppliers, and materials development engineers can use this simple but precise device for addressing thermoforming material- and process-related issues. With further

² Ed. Note: Commercially available PC is normally an amorphous polymer with a glass transition temperature of around 150°C.
effort, a built-in predictive model can be incorporated to allow efficient process set-ups.

References


7. B. Hagemann and P. Eyerer, “Improving industry through technical development.”


We’ve all heard the argument that filled plastics heat at different rates than unfilled plastics. This Industry Practice article explores this argument with simple examples. The theoretical analysis will appear in a subsequent Technical Article in TFQ.

We need to make some simplifying assumptions. Consider our filler to be TiO₂, either an opacifier at a relatively low loading of 10 wt% (Example A) or a filler at relatively high loading of 40 wt% (Example B). For simplicity, consider the particle shape to be spherical with a particle size of 10 microns. Consider the plastic to be generic. We’ll need to make additional assumptions later.

Some simple arithmetic, first.

**Volume Fraction:** The filler volume fraction is given in terms of weight fraction as:

\[ \text{Volfract} = \frac{\text{wtfract}}{\left(\frac{\text{density}_{\text{polymer}}}{\text{density}_{\text{filler}}}\right)} \]

The density of TiO₂ = 4.36. The density of our generic plastic is 1.0, say. The volume fractions of our two loadings are:

Example A: \( \text{Volfract} = 0.10 \times \left(\frac{1}{4.36}\right) = 0.0235 \) or 2.35 vol%

Example B: \( \text{Volfract} = 0.40 \times \left(\frac{1}{4.36}\right) = 0.0917 \) or 9.17%

**Plastic-filled Density:** The density of a filled plastic is given as:

\[ \frac{1}{r_{\text{filled}}} = \frac{\text{wtfract}}{r_{\text{filler}}} + \frac{(1-\text{wtfract})}{r_{\text{plastic}}} \]

Example A: \( r_{\text{filled}} = \frac{1}{[0.10/4.36 + 0.9/1]} = 1.08 \)

Example B: \( r_{\text{filled}} = \frac{1}{[0.40/4.36 + 0.6/1]} = 1.45 \)

**Specific Heat:** The specific heat or heat capacity is a measure of the amount of heat required to heat the plastic to its forming temperature. The greater the specific heat, the more energy is required.

\[ \text{SpHt}_{\text{filled}} = \text{Volfract} \times \text{SpHt}_{\text{filler}} + (1-\text{Volfract}) \times \text{SpHt}_{\text{plastic}} \]

The specific heat of TiO₂ is 0.2. The specific heat of neat generic plastic is, say, 0.4.

Example A: \( \text{SpHt}_{\text{filled}} = 0.0235 \times 0.2 + (1-0.0235) \times 0.4 = 0.394 \)

Example B: \( \text{SpHt}_{\text{filled}} = 0.0917 \times 0.2 + (1-0.0917) \times 0.4 = 0.382 \)

**Thermal Conductivity:** The equation for thermal conductivity of a filled plastic is relatively complex. It is the Nielsen equation, used to determine, among other things, the mechanical properties of composite systems.

\[ \frac{k_{\text{filled}}}{k_{\text{plastic}}} = \frac{1+AB\text{Volfract}}{1-BQ\text{Volfract}} \]

\[ B = \frac{(k_{\text{filler}}/k_{\text{plastic}}-1)}{(k_{\text{filler}}/k_{\text{plastic}}+A)} \]

\[ Q=1+[(1-V_{\text{Volfract}})/V_{\text{Volfract}}]v \]

\[ A=kappa_{E}-1 \]

\[ V_{\text{Volfract}} = 0.6 \text{ (random spheres)} \]

\[ kappa_{E} = 2.5 \text{ (spheres)} \]

The most important aspect of this equation is the term, \( V_{\text{Volfract}} \). This is the maximum packing that can be achieved with the particular filler. For this case, we assume that we have uniformly dimensioned spheres. As a result, \( A = 1.5 \).

Example A: \( Q = 1 + [(1-0.6)/0.62]0.0235 = 1.026 \)

\[ B=(40/0.4-1)/(40/0.4+1.5) = 0.975 \]

\[ k_{\text{filled}}/k_{\text{plastic}} = (1+1.5x0.975x0.0235)/(1-0.975x1.026x0.0235) = 1.059 \]

Example B: \( Q = 1+1.11x0.0917 = 1.102 \)

\[ B = 0.975 \]

\[ k_{\text{filled}}/k_{\text{plastic}} = (1+1.5*0.975*0.0917)/(1-0.975*1.102*0.0917) = 1.258 \]

Now we can summarize the changes in thermal properties because of the presence of TiO₂ in the plastic.
As expected, increasing filler concentration results in increased filled polymer density. The specific heat does not substantially decrease. Therefore, the total amount of energy required to raise a specific volume of filled plastic to its forming temperature (that is, its specific gravity times its density or its heat duty) increases substantially with increasing filler concentration. In the case of 40 wt% TiO₂, the additional heat duty is 38.5%.

In short, the more rock there is, the more energy it takes to heat it.

Now we explore another facet of this question: Does the presence of filler change the way in which the plastic receives radiant energy? To answer this question, we need to consider geometry. This time, we consider a cube of plastic, T units on a side. Assume for the moment that the filler is compressed into a cube, t units on a side. What is the volume occupied by the filler?

A simple form of the equation is:

\[ A_{filler} = \left( \frac{t}{T} \right)^2 = (Volfrac)^{2/3} \]

Example A: \( A_{filler} = (0.0235)^{2/3} = 0.082 \) or 8.2% of the surface is filler

Example B: \( A_{filler} = (0.0917)^{2/3} = 0.203 \) or 20.3% of the surface is filler

We now need to make some simplifying assumptions about the volumetric distribution of the particles in the plastic matrix. Recall that our particle size is 10 microns. We assume that the particles are uniformly distributed throughout the volume. As a result, the first 10 microns of the filled plastic are composed of about 8% filler for the 10 wt% dosage and about 20% for the 40 wt% dosage. For the rest of this journey, consider only the higher dosage case.

As we know from FTIR graphs, all plastics are semi-transparent to incident far-infrared radiation. Consider the case where the average transmission of radiant energy though the first 10 microns of plastic is 50%. This means that 50% of the incident energy is absorbed by the first 10 microns of plastic and 50% is transmitted to the next 10 microns. Furthermore, assume that in the next 10 microns of plastic, 50% of that energy is absorbed and 50% is transmitted to the third 10 microns of plastic. And so on.

As we said, we are using the 40 wt% dosage case. Assume that the filler particles reside in 10 micron layers throughout the plastic. As a result, 20% of the first 10 microns of plastic contain filler particles. As does the next 10 microns and the next 10 microns, and so on. For this analysis, consider that all the incoming radiation that impinges on the filler particles is totally absorbed, to be ultimately conducted into the plastic.

Now consider inbound radiation to the first 10 microns of filled plastic. That portion that impinges on the filler is completely absorbed. That portion that impinges on plastic is only 50% absorbed, as we assumed above. This is written as:

**1st Layer:**

Absorbed: \( \text{inbound radiation} \times \text{filler area} + \text{absorbed portion} \times \text{open area} = \)

Transmission: \( \text{filler block of all radiation} \times \text{filler area} + \text{transmitted portion} \times \text{open area} = \)

Absorbed: \( 100\% \times 20\% + 50\% \times (100\%-20\%) = 60\% \)

Transmitted: \( 0\% \times 20\% + 50\% \times (100\%-20\%) = 40\% \)

Now for the second layer, only 50% of the original radiation is available. And an additional 20% of the surface area is blocked by filler particles. So this is written as:

**2nd Layer:**

Absorbed: \( 50\% \times 20\% + 50\% \times 50\% \times (80\% - 20\%) = 25\% \)

---

1 This is not quite correct, because we are not properly taking into account the volume occupied by the filler. But, considering all the other assumptions …
Transmitted: 0% of 20% + 50% of 50% of (80% - 20%) = 15%

On to the third layer. Only 50% of the 50% of the previous radiation is available for absorption and transmission. And an additional 20% of that surface area is blocked. So we write:

\[
T_{\text{total layer}} = \begin{array}{cccccccc}
\text{Filler Conc} & 1^{\text{st}} & 2^{\text{nd}} & 3^{\text{rd}} & 4^{\text{th}} & 5^{\text{th}} & 6^{\text{th}} & 7^{\text{th}} \\
0 & 50\% & 75\% & 87\% & 94\% & 97\% & 98\% & 99\% \\
40 & 60\% & 85\% & 95\% & 99\% & 100\% & \\
\end{array}
\]

It is apparent that the filler blocks radiation transmission into the polymer. Therefore, all things being equal, the sheet surface should heat at a rate that increases with increasing filler concentration. And, because infrared thermometers measure sheet surface temperature, filled polymers appear to heat faster than unfilled polymers.

But wait. As we saw earlier, the thermal conductivity of the filled plastic increases with increasing filler dosage. This means that even though the surface of a filled plastic receives more energy than that of an unfilled plastic, the energy is conducted into the interior of the plastic at a faster rate.

**Conclusion**

There are two general aspects to energy input to filled plastics. The first is that the energy needed to raise a filled polymer to its forming temperature increases with increasing filler concentration. The primary reason is that the plastic density increases with increasing filler concentration.

The second is that at the same energy input rate, filled polymer surfaces absorb more energy than unfilled polymer surfaces. If this were the only effect, we would see filled polymer surfaces heating at a more rapid rate than those of unfilled polymers. And normally we do. However, filled polymers have higher thermal conductivities than unfilled polymers. This means that for filled polymers, the energy near the surface is conducted to the interior at a faster rate than that for unfilled polymers. This is a very important compensating factor. On balance, a polymer heats at about the same rate whether neat or filled.
Distortion Graphics for Thermoformed Parts – Elastic Image, A Development of Rose-Hulman Institute of Technology

Who are we?

We are graphics and plastics professionals backed by a strong corps of engineers and software scientists. We have developed an automated digital solution for distorting graphics for pre-decorating plastics. We are partnered with Rose-Hulman Ventures (RHV), a technology incubator arm of Rose-Hulman Institute of Technology in Terre Haute, IN. Together we have developed proprietary software and hardware to expand capabilities in the manufacturing of decorated plastic products for a wide variety of applications. Our partnership with RHV allows us to accelerate our technical development through R & D and engineering initiatives. As a result, EI has established the benchmark for exceptional quality in pre-decorated plastics.

What are we selling?

We deliver the ability to advance manufacturing capabilities for decorating formed plastic products. We provide the means for manufacturers to eliminate the risks and design limitations inherent in the outdated trial-and-error methods for distorting graphics. EI provides speed-to-market in both the development and production phases. We drive value at every touch-point in the cycle from design concept to final delivery. Designers, tool makers, plastics companies, graphics producers, and forming manufacturers are embracing the EI technology. We enable clients by providing a unique platform for increased creativity and design flexibility. We develop new products that deliver increased value-added. Our technology offers powerful differentiation opportunities for our customer’s products and brands.

How was it developed?

The current technology is a proprietary integrated suite of hardware and software comprised of machine vision-based data collection and graphic distortion computation. It is the result of the marriage of development between two groups of software scientists and engineers. Each group tackled part of the challenge. An RHV group developed the 3D scanning solution that quantifies material stretch while another developed the graphics distortion package. These two platform technologies were brought together initially in 2003. In parallel with commercial rollout, EI has continued to improve both platforms and is now in its fourth phase of development. EI and RHV continue to commit resources against the ongoing development and evolution of the technology.

How does it work?

Unlike attempts to develop distortion solutions through predictive means, the EI solution is based on capturing the specific surface dynamics of a
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History of Thermoforming – Part III

BY STANLEY R. ROSEN, PLASTIMACH CORPORATION, LAS VEGAS, NEVADA

Ed. Note: The philosopher Santayana said “Those who cannot remember the past are destined to repeat it.” Stan Rosen is undertaking a prodigious project – identifying the pioneers who laid the foundations of the industry we know so well. Although shaping of sheet extends back to pre-history – oil-heated and shaped tortoise shell and steam-heated and shaped wood. In TFQ 24:3, Stan started his history with developments in the 1930s. We hope you are enjoying the trip!

Mechanically Forming Thermoplastics Parts Prior to the Thermoforming Age – Part One

Commercial thermoforming machinery and forming technology developed quickly in the U.S. during the early 1950s. Prior to that date, thermoplastics were most often formed mechanically using various methods by firms specializing in providing formed plastic products to their customers. These mechanical forming techniques were slow, labor intensive, and did not always provide reproducible results. Several visionary companies during this era invested in the design of thermoforming equipment to suit their own needs. However these machines were not sold on the open market. Borkland Laboratories licensed vacuum forming equipment in the late 1940s. Plax Corp. built and used automated thermoforming machines in the 1930s and Plaxall Corp. apparently built inline thermoformers for their own production in the early 1950s. A majority of the plastics fabricators continued to use mechanical forming techniques until commercial vacuum forming equipment was first publicly demonstrated at the National Plastics Exhibition in March 1952. Within one year, thermoforming activity expanded explosively as equipment and technical information became available to industry.

Mechanical forming of thermoplastic sheet borrowed some of the methods which were in use in the metal working and paper-box making industries. A metal deep drawing technique for fabricating a pot or pan from metal blanks was modified to process celluloid into seamless transparent packaging from individual plastic blanks. Paper box manufacturers employed die-cutting, creasing, bending and the cementing of box corners for their products. Many of these paper box procedures were suitable for the production of plastic boxes and lids. Other forming processes modified from the glass blowing and metal forming industries were adapted to accommodate the physical properties of plastics materials.

Celluloid, a combination of cellulose nitrate, camphol and other chemical additives, was the first commercial plastic sheet available in 1868. Equipment to fabricate the sheet used a “blow form process” in which two heated celluloid sheets were placed between female molds and when the press was closed the cavity perimeter edges were trimmed and heat sealed together. Steam pressure then entered between the sheets to force the pre-heated plastic into the cavities. (Fig. 1, Fig. 2).

Figure 1. Blow-form press.

Figure 2. Blow-form mold.
This process, which is similar to modern twin sheet-forming or blow molding, was used for production of double-faced parts such as balls, baby rattles, etc., starting in the 1890s. The same process could form one heated sheet into a female cavity producing shallow formed open-faced parts similar to a blister packaging component.

The city of Leominster, Massachusetts became the hub of the celluloid era (1900-1920) manufacturing activities and it pioneered in all types of plastics fabrication, especially blow forming. The ancillary components for manufacturing finished plastics components such as molds, presses and dies were manufactured here and sold worldwide. This pioneering city of the plastics industry is the home of the National Plastics Center and Museum where early plastics processing equipment is on display.

Manual deep drawing of thermoplastic sheets is described in a 1937 patent by William E. Helmstaedter, of the Celluloid Corp. (later Celanese Corp.) as follows (Fig. 3):

A temperature-controlled “former assembly” consisting of a male cavity and a hardened cutoff punch is mounted to the top moving platen. The punch is located on the back face of the male cavity. The opposite stationary platen contains a heated die whose interior edge is rounded slightly to assist plastic flow between the die opening and onto the moving former. A heavy hold-down plate (much like a clamp frame), which applies its weight to prevent the sheet from wrinkling during forming, allows the plastic flange to slip between the hold-down plate and the face of the hot die. This heated flange area provides the necessary additional material to form the finished part. Blanks thicker than .015 inch (.38 mm) require preheating in an oven and then are manually transported quickly to the forming press. Unlike the thermoforming process, where the heated sheet thins as it is being formed, deep drawing “steals” material from the flange as it slides between the former and the die and produces a fairly uniform sidewall.

Trimming and heat sealing of the finished drawn part edge takes place when the punch strikes the top surface of the die, causing the formed part to be trimmed by a heat pinch-off action. The more traditional punch and die design which is in more common usage in the industry allows the punch to cut through the plastic and enter the die cavity. Helmstaedter stated in the patent that a small temperature differential between a heated traditional punch and die could cause trimming problems. If the punch is cooler than the die, the tool clearance will increase and possibly cause a rough trimmed edge. A punch which is hotter than the die can reduce the clearance to zero causing a die smashup. These facts are recognized on modern thermoformers that form and trim in the same station using a punch and die, since this type of tooling receives considerable heat from the hot web. The control system of these newer machines can shut down the equipment if they detect an unsafe temperature differential between the two halves of the tool.

[To be continued]

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Fig. 1 and Fig. 2 - Plastics History U.S.A., J. H. Dubois – 1972, pgs. 45 and 347.

Fig. 3 - Manual Deep Drawing of Plastics Packaging, W. E. Helmstaedter, Patent #2,255,116 filed 1-21-1937 assigned to Celluloid Corp., Newark, N. J.
Some time ago, we discussed shrinkage and warpage. At that time, we pointed out that plastic, like most other materials, increases in volume when heated and decreases in volume when cooled. And we said that to form the desired shape, the hot plastic is pushed against a cool mold surface. It follows that as the plastic cools, it shrinks. But the mold doesn’t change in dimension. If the mold is male or positive, or if even a portion of the mold is male or positive, the plastic will shrink onto the mold surface. And if the mold is not properly designed, we will have a devil of a time getting the part off it. Thus we face the subject of draft angles.

**Draft Angles – Defined**

The best definition of a draft angle is the angle the mold wall makes with the vertical. If the mold wall is vertical, the draft angle is zero. Recall that most thermoforming molds are single-surfaced. That is, the sheet is pulled into or over a single mold surface. For draw-down into a female or negative mold, the sheet is constrained on its outer surface by the mold. As a result, when the sheet cools, it tends to shrink away from the mold surface. As a result, it is entirely feasible to thermoform into a female mold having zero draft angles. Most part designers prefer a slight draft angle, say 0° to 2°, “just in case.” The average is generally 1/2° to 1°.

On the other hand, when the sheet is drawn over a male or positive mold, it is constrained on its inner surface by the mold. As a result, when the sheet cools, it tends to shrink onto the mold surface. To release the part from the mold, it is necessary to provide a draft angle on the vertical mold surfaces. The amount of draft depends strongly on the volumetric change in the polymer. If the polymer is amorphous – PS, PVC, PC – the draft angle may be no more than 2° to 3°. If the polymer is crystalline – PE, PE – the draft angle may be in excess of 5°. The average is generally 4° but the designer must be alert to effects of temperature variation and recrystallization rates.

A textured surface requires an increase in draft angle. It is recommended that the draft angle be increased at least 1° for every 0.2 mils [0.0002 in or 5 microns] in texture depth. Keep in mind that increasing applied pressure, sheet temperature, and mold temperature will result in greater penetration of the sheet into the texture.

**What About Parts With Male and Female Components?**

Multiple-compartment trays and pallets can pose serious drafting issues. Consider a female cavity bordered by two male segments. The sheet will attempt to shrink away from the female mold surface but onto the male segments. Excessive draft on the male segments may allow the sheet to release from the female mold surface before the sheet has replicated the mold surface. On the other hand, inadequate draft on the male segments may allow the sheet to satisfactorily form the female mold surface, but the sheet may “lock” onto the male segments. The problem is exacerbated when molding compartment trays where the male portions are

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1. These parts are sometimes called androgy nous, meaning that they have both female and male characteristics.
2. Exacerbate: To aggravate.
interrupted. Essentially interrupted walls in the molded part. In addition to the shrinkage issues, interrupted male segments may also be sources of internal webbing3.

**How Serious is the Draft Problem?**

The draft angle can lead to serious dimensional changes in the formed part. Consider a simple example, a 10-inch male mold. The vertical wall is 1 inch wide at the top. Consider a draft angle of 5°. The width at the bottom of the vertical wall is determined as follows:

The increased width on one side is $10 \times \tan 5° = 0.875$ in. The total width at the bottom is then $1 + 2 \times 0.875 = 2.75$ in.

This is a substantial dimensional change in the thickness of the vertical wall.

**When is the Draft Angle Not a Draft Angle at All?**

When it is used for something else. The classic example is the drink cup. The sidewalls are tapered as much as 20° for stacking purposes, not shrinkage. In multi-compartment parts, care must be taken in the design to accommodate both the draft angle required for shrinkage and the necessary stacking taper. Stacking lugs, stand-offs, or rings are often designed into complex parts, simply because it is not always possible to predict the exact local shrinkage. ■

**Keywords:** draft angle, taper, shrinkage

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**BOOK REVIEW**


I am always skeptical of the schemes proposed in the help guides for managers, dozens of which are published each year. Most of these repeat the same or similar mantra regarding manager-employee goal setting and review procedures. I am always reminded of the Dilbert cartoon where his pointy-haired boss (aka PHB) presents Dilbert with a long list of projects. When Dilbert asks him which are A priority and which are B and C priority, PHB tells him that this is the A list and that he has yet to make up the B and C list.

Michael Hill is VP of an industrial distribution center with five branch locations and over 100 employees. He has been a member of SPE for more than 20 years and is past president of the International Association of Plastics Distributors. He has an MBA from St. Bonaventure University. Mr. Hill has written a modest book with a very modest goal and has published it at a very modest price. According to the introduction, it “deals with teaching managers to achieve their goals by using measurable criteria to evaluate employee performance.” The book has 11 chapters – Problems in Today’s Climate, What a Company Should Do, Setting Your Evaluation Goals, Measuring, “Your” Evaluation, Pre-Review Tips, Examples, The Actual Review, Future Encouragement, When All Else Fails, and Final Word on Measuring.

In addition to being very readable, the book contains many quotable statements. For example:

“A mediocre product … with good people will easily outperform a great product marketed by a weak organization.”

“A goal, by definition, needs to be measurable …”

“Don’t risk losing your investment in your employees due to poor management.”

“Reviews based on measurable criteria hold no surprises for the employee …”

“Always be on the lookout for measurable criteria …”

“… every company wants … employees [to accept] responsibility for their actions, and in fact [to review] themselves.”

Hill argues that performance review and salary review should be separate entities. And that performance review has three components – management preparation, human resource input, and employee preparation. His mantra can probably be summarized by this:

“Without a yardstick there is no measurement. And without measurement, there is no control.” Toward this, he outlines a five-step program for achieving quality employee reviews.

Hill’s book is a fast read, with his thesis outlined only after he has “set the table” by discussing the failure aspects of other types of review. The reader should be fully aware that Hill’s proposed program needs to be designed by each manager to meet the needs of his/her employee team. And that this design is the sole responsibility of the manager. Hill’s thesis is technically viable so long as the manager-employee structure remains stable over an extended period of time.
But this reviewer sees three aspects of the proposal that remain largely unaddressed. The first deals with quixotic managers who consider reorganization as part of their obligation. Reorganizing employees and employee responsibilities on a frequent basis does not lead to development of dedicated people. The second deals with the reality of today’s market. Very often, companies have extremely skilled and dedicated people who are working in areas being marginalized by shifting markets. Acquisitions, mergers, and buyouts enable to company to rapidly shift to the newly emerging markets, but unfortunately often force the company to surplus their best workers who simply cannot be retrained fast enough. And the third deals with rating managers. Too often, employees have no way of measuring the effectiveness of their manager to manage them. Managers may be oblivious to mannerisms or actions that, while “politically correct,” irritate and annoy their people. This is particularly true of managers who manage by the book rather than lead by example.

So, is this a book that every manager should read? Sure. It has far more substance and is much easier to digest than do some of the weekly columns in the Wall Street Journal. But it is this reader’s belief that good managers should purchase copies for each of their employees. The employee would then be aware of the reasons behind the five-step criteria being used to rate him or her. After all, even Hill says that “[w]hen company information and company goals are shared and agreed upon, everyone wins.”

I rate this modest effort a strong four-and-a-half books out of five.

~ Jim Throne, Tech Editor
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27 Thermoforming QUARTERLY
January is National Mentoring Month. There are many ways to become involved with mentoring. One of the best is for companies to offer internships to university students studying for a career in plastics. Student internships might help slow the long-term erosion of the manufacturing sector in the U.S., and there are many other benefits as well. What are those benefits? Ask Joe Peters, president of Universal Plastics in Holyoke, Mass. Ask Lucas Stallbaumer, a student of plastics engineering technology at Pittsburg State University in Pittsburg, Kansas. Here is their story.

Lucas Stallbaumer wanted to know what he was getting himself into. At the end of his junior year at Pittsburg State – pursuing a bachelor’s degree in plastics engineering technology, with an emphasis in manufacturing – Lucas decided to apply for a summer internship. He desired “hands-on” working experience at a plastics company. Lucas also wanted a change of scenery: he had never seen the ocean.

When Bill McConnell of McConnell Co., Inc., a member of the Board of Directors of SPE’s Thermoforming Division and a member of Pittsburg State University’s Plastics Advisory Council, spoke to Lucas and fellow students enrolled in plastics technology classes, he provided a list of companies specializing in thermoforming that might welcome student interns. Lucas emailed all the companies on the list. He received responses – and offers of internships – from two.

Lucas accepted the offer from Joe Peters, president of Universal Plastics in Holyoke, Mass., and his summer-of-2005 internship began. On May 29, Lucas boarded Southwest Airlines flight 132 K in Kansas City, bound for Massachusetts. His mother was not as excited about the trip as Lucas was. “My mom cried most of the way to the airport,” he recalls. Rich and Sue Peters (Joe’s brother and sister-in-law) shared their home in Westfield, Mass., with Lucas for the summer. “I was welcomed and treated as part of the family. For this I am really thankful. It sure beat staying in a dorm room,” says Lucas.

At Universal Plastics, Lucas settled in with his own desk and computer in the engineering department. Joe Peters wanted to make sure that during the summer, Lucas’s work duties took him into every area of the shop – from actually forming some parts to working with tooling and secondary operations. “I wanted him to work with engineers, supervisors, and line employees,” Joe says. Lucas was involved in new and ongoing projects, and was given a number of tasks, such as helping to design a package, testing designs, and sourcing materials and hardware for products the company manufactures.

His number-one job, reports Lucas, was assisting the company’s forming department by creating computer spreadsheets that listed data pertaining to the forming of parts. The easy accessibility of Lucas’s electronic data sheets eliminated the need to shuffle through piles of unorganized papers in search of a particular document (if indeed one was to be found) and greatly facilitated the search for information on a particular part to be set up on a machine for production. Working on the spreadsheets familiarized Lucas with the materials being used, heating and cooling times, mold temperatures, forming pressures, and the PLCs (programmable logic controllers) of various machines, he says. Joe reports that Lucas’s computer skills were highly valuable to the company: “He was in demand when others found out that he was great at designing forms.”

The most important thing Lucas learned during his internship: in the real world of producing parts, “things can become very frustrating very fast if things do not go right, but you have to keep your cool and get the job accomplished.” In helping with the thermoforming of 5-inch polyurethane cones, for example, Lucas observed that frequent and capricious changes in processing parameters (e.g., humidity, temperature, material thickness, and air pressure) make it challenging to produce consistent web-free parts that are neither too thin nor too short, and to produce them on time. Lucas was also absorbed in figuring out the process needed to apply large printed vinyl stickers to street signs. The stickers had to be perfectly centered and straight,
with no distortions in the print at all and no air bubbles or water intrusion, which would void the manufacturer’s warranty. It was a hurry-up job to meet the customer’s demand for a short turnaround time.

In an academic setting, one might encounter a difficult problem, postpone a solution, and return to deal with it another day. In the business world, walking away even temporarily from an unsolved problem is not an option. An idle machine shrinks a company’s profits, and poor-quality parts or parts delivered late make for disgruntled customers, who might take future business elsewhere. Lucas points out: “So your company loses money and you could lose your job.”

Throughout his internship at Universal Plastics, Lucas says, he learned lessons he did not expect to. “I learned the key aspects of business – from engineering to sales, research, forming, machining, quality control, and shipping. I learned a lot from all the steps involved in the entire business.” Lucas also established business relationships and friendships with his coworkers that he thinks will last a lifetime. “I would suggest more students take part in an internship before they get into the workforce, to see what they are actually getting themselves into,” he says.

Lucas thinks more companies should approach local colleges to seek interns, to train students in hopes that upon graduation they will join the staff as permanent employees. “That way,” he says, companies “will not have to spend as much time or money familiarizing them with procedures, processes, machines, people, and other things that make a company run.”

Joe Peters says, “Unfortunately, kids today are not being exposed to manufacturing and engineering as a career path. They are not aware of the technology involved and the many rewards of creating and manufacturing products. Giving them an opportunity to spend some time [in the work environment] is invaluable in helping them make their career decisions.” Furthermore, he adds, in the U.S. the reality is that we have to do as much as we can to promote manufacturing, which is quickly diminishing as an economic force in our country. Helping students acquire first-hand experience is an extremely valuable tool.

By the way, Lucas did get to see the ocean – at the Peters family’s vacation home in Maine. He walked the beach, dined on lobster, and sailed on the Atlantic. He helped hoist the mast and sail the boat, and even accompanied the Peters’ son Andrew on a flying lesson. Andrew’s aerial stunts – spinning in circles, ascending straight up, and killing and recovering the engine – made him a bit dizzy, Lucas admits, but the scenery below was beautiful.

Joe Peters, president of Universal Plastics, invited Lucas Stallbaum, a student of plastics engineering technology at Pittsburg State University, Kansas, to spend the summer as an intern at his company in Holyoke, Massachusetts.
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Just send Jim Throne a fax at 727-734-5081, outlining your tip in less than a couple hundred words. You can include drawings, sketches, whatever. Thanks!
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